



COST OF CO₂ CAPTURE FOR SMALL-SCALE DISPATCHABLE POWER GENERATORS

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Introduction

Open-cycle gas turbines (OCGT) are quick starting dispatchable generators that provide system security and flexibility; aiding in the uptake of more renewable and nuclear power generation sources [1]. However, in order to reach Net-Zero by 2050, these peaking plants will require Carbon Capture and Storage (CCS). Therefore, this study looks at the cost of incorporating post-combustion capture (PCC) on an OCGT power plant. Study objectives:

- Calculate the levelised cost of electricity (LCOE) for an OCGT+CCS system.
- Calculate the cost of CO₂ avoidance (CCA) for an OCGT+CCS system.
- Compare OCGT+CCS against other low-carbon power sources.

IS DISPATCHABLE GAS-CCS AFFORDABLE?

Process

This study utilises process models developed in our previous studies, and extracts the key operating and design parameters required in the economic model. The OCGT+CCS plant (Figure 1) consists of:

- **Power plant** – 10.4 MWe OCGT with highly transient operation, producing 33.8kg/s flue gas (6.78 wt.% CO₂) [2].
- **CO₂ capture plant** – benchmark 30 wt.% MEA with 92.5% capture rate [2].
- **CO₂ conditioning plant** – 4 stage compression system, producing a CO₂ stream at 111 bar and 50 ppm moisture, ready for pipeline transportation [3].

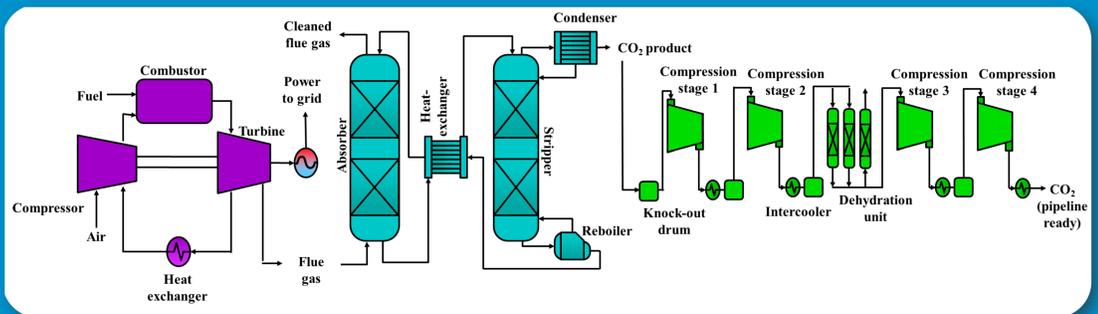


Figure 1: Flowsheet for an OCGT+CCS power plant, highlight the major pieces of equipment

Cost Breakdown

To economically evaluate OCGT+CCS, you need to identify the major pieces of equipment and calculate:

- Purchased equipment cost (PEC) – using correlations from Towler & Sinnott [4].
- Total capital cost (TCC) – using correlations from Chauvel et al. [5].
- Fixed operating and maintenance (FOM).
- Variable operating and maintenance (VOM).

FOM and VOM are calculated using data extracted from the process models.

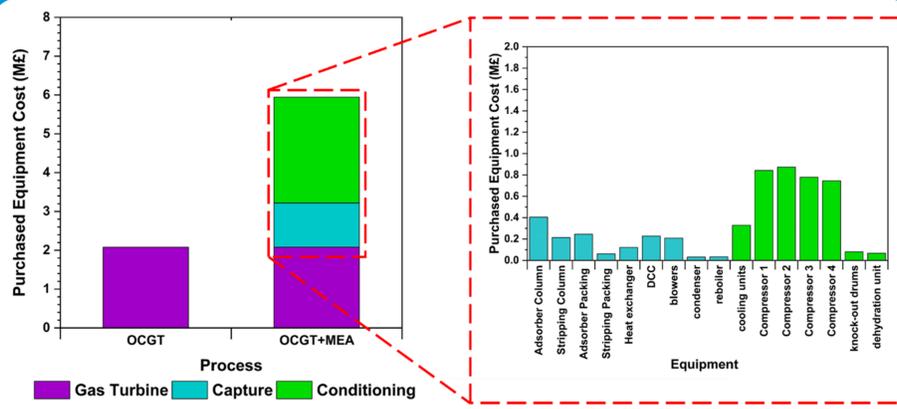


Figure 2: PEC breakdown for an OCGT power plant with and without CO₂ capture and conditioning

The TCC for the OCGT is 6.53 M£ or 628 £/kW, comparable to estimates from industry. The total PEC for the OCGT, MEA, and conditioning plants are 2.08, 1.55 and 2.32 M£, respectively. As shown in Fig. 2, the compressor costs dominate the PEC; indicating, these small-scale emitters would benefit from sharing the conditioning load or incorporating CO₂ utilisation.

LCOE and CCA

The LCOE is the sum of the net present value (NPV) of costs divided by the sum of the NPV of electricity generated and sold:

$$LCOE = \frac{NPV_{total\ costs}}{NPV_{generation}} = \frac{\sum \left(\frac{TCC_t}{(1+r)^t} + \frac{FOM_t}{(1+r)^t} + \frac{VOM_t}{(1+r)^t} \right)}{\sum \left(\frac{net\ electricity\ generated_t}{(1+r)^t} \right)} \quad [1]$$

Where r is the discount rate, and t is the time period. Once the LCOE is calculated for the reference (ref) case and the OCGT+CCS (CCS) case, you can then calculate the CCA:

$$CCA = \frac{(LCOE)_{CCS} - (LCOE)_{ref}}{\left(\frac{tCO_2}{MWh} \right)_{ref} - \left(\frac{tCO_2}{MWh} \right)_{CCS}} \quad [2]$$

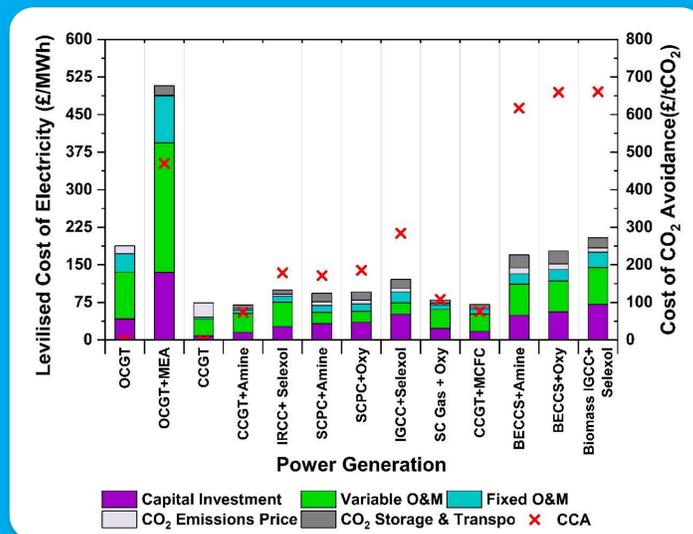


Figure 3: LCOE and CCA comparison between OCGT+CCS and other forms of low-carbon power from BEIS [6]

Table 1 highlights the key performance indicators (KPI) of OCGT+CCS. The significant increase in VOM and FOM (electricity, heat duty, and solvent stock) makes the LCOE of OCGT+CCS much higher than other low-carbon sources (70 -204 £/MWh). However, the CCA for OCGT+CCS is lower than bioenergy with CCS (BECCS) which ranges between 617-661 £/tCO₂.

Table 1: KPIs for OCGT+CCS

| KPI | OCGT | OCGT+CCS ^a | OCGT+CCS ^b |
|---|--------|-----------------------|-----------------------|
| Net power output (MWe) | 10.4 | 9.11 | 9.11 |
| CO ₂ emission (tCO ₂ /yr) | 12,400 | 981 | 981 |
| LCOE (£/MWh) | 172 | 487 | 507 |
| CCA (£/tCO ₂) | - | 470 | 448 |

Note: ^a carbon price set to zero, ^b carbon price set to £21.70/tCO₂ BEIS [6]

Conclusion

- Including CCS for dispatchable gas turbines increases the LCOE by **183-195%**.
- The CO₂ conditioning plant accounts for **60%** of the additional capital investment.
- In order to achieve **Net-Zero by 2050** cost effectively, future work should investigate:
 - Alternative forms of dispatchable power, e.g. energy storage, H₂ turbines, pumped hydro.
 - Different CO₂ capture and utilisation technologies, e.g. fuel cells or chemical looping.
 - Integration of small-scale utilisation options.

Economic Issues with dispatchable OCGT+CCS:

- **Economies of scale** – the small plant size means the cost per MWh is a lot higher.
- **Low capacity factor** – OCGTs are peaking plants and they operate <1,500 hours annually, significantly less than other power sources.

References:

- [1] J. Stern, "The Future of Gas in Decarbonising European Energy Markets: the need for a new approach," Oxford Institute for Energy Studies, Oxford, 2017
- [2] M. D. Wilkes, S. Mukherjee and S. Brown, "Transient CO₂ capture for open-cycle gas turbines in future energy systems," Energy, p. 119258, 2021
- [3] M. D. Wilkes, S. Mukherjee and S. Brown, "Linking CO₂ capture and pipeline transportation: sensitivity analysis and dynamic study of the compression train," International Journal of Greenhouse Gas Control, vol. 111, p. 103449, 2021
- [4] G. Towler and R. Sinnott, Chemical Engineering Design: Principles, Practice and Economics of Plant and Process Design, 2nd ed., Oxford: Elsevier, 2012
- [5] A. Chauvel, P. Leprince, Y. Barthel, C. Raimbault and J.-P. Arle, Manual of Economic Analysis of Chemical Processes: Feasibility Studies in Refinery and Petrochemical Processes., McGraw-Hill, 1981
- [6] BEIS, "Assessing the Cost Reduction Potential and Competitiveness of Novel (Next Generation) UK Carbon Capture Technology," UK Department for Business, Energy & Industrial Strategy, 2018